

Energy control strategies for the Fuel Cell Hybrid Power Source under unknown load profile



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ABSTRACT

Four new energy control strategies are proposed here for the Fuel Cell Hybrid Power Source (FCHPS) used in stationary and mobile FC application (such as the FC backup source for a smart-house and FC vehicle, respectively) based on the Load Following (LF) control and Maximum Efficiency Point Tracking (MEPT) control of the fueling rates. The LF control approach is used to design simple strategies of the Energy Management Unit (EMU) that will assure a charge-sustaining mode for the batteries stack of the Energy Storage System (ESS). If a fueling rate is controlled based on the LF strategy, then the other is controlled based on MEPT strategy in order to maximize the FC net power available. The advantages of the proposed EMU strategies during an unknown load cycle are comparatively shown.

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1. Introduction

In last decade the FC applications try to penetrate into the specific market and the FC issues are extensively revised in Refs. [1,2], as good references to start a FC system implementation. Nevertheless, the EMU (Energy Management Unit) strategies for energy management and optimization are still at an early stage for the FC applications [3,4]. Consequently, it is a challenge for the designers to develop an EMU strategy to optimize the operation of FC stack [2] and increase the lifetime of FCs and batteries [3], these being the main objectives in designing of a FCHPS (Fuel Cell Hybrid Power Source). Thus, several EMU strategies have been proposed based on the power flow balance to control the distribution of power between the two energy sources (FC and ESS (Energy Storage System)) and the load [5], but none based on the LF (Load Following) control that is proposed here to optimize the size of the ESS. An equivalent consumption minimization and a real time optimal EMU strategy based on the dynamic load strategy are presented in Refs. [6,7], but the FC stack doesn't operate close to the MEP. A MEPT (Maximum Efficiency Point Tracking) strategy is put forward here to increase the efficiency of the whole FCHPS. The power profile requested by the equivalent load will be split into

three frequency components based on the wavelet or other filtering transformation [8,9], but this cannot be made in real-time, without increasing the control circuit complexity. The idea to use the low frequency power component as the control reference for the FC system (in order to protect it against sharp changes on real load cycles [8]) is very good, but here it will be used in a different manner, which is easier to be implemented.

All strategies mentioned above were tested under standard load cycles, but in general the real load profile is unknown. Thus, more input and state variables must be used in EMU strategy (with expense of increasing the EMU complexity), if the LF control proposed here is not used. For example, if both batteries and ultra-capacitors stacks States-Of-Charge (SOC) are considered and the power profile of the load cycle is unknown, then the basic rules of the fuzzy logic control proposed in Refs. [10,11] will become too complex compared to the LF control proposed here. Note that other two EMU strategies based on fuzzy logic controller are proposed in Refs. [10,12] to include the dynamic restrictions of the power sources and regenerative braking power flow based on new input variables considered. The LF control proposed here is based only on the load power, so this has some advantages compared to these proposals. Thus, it is worth to mention the two main advantages obtained based on LF control put forward here: (1) the EMU strategy is very easy to be implemented and (2) the size of battery stack is minimized (because the battery SOC is maintained almost constant during a load cycle).

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A perturbation approach to minimize the hydrogen consumption in Polymer Electrolyte Membrane (PEM) FC systems was introduced in Ref. [2] and the main drawback of this technique (related to the fixed values of the algorithm parameters) is solved here based on the Extremum Seeking (ES) control scheme [13] used for the MEPT algorithm. The hydrogen consumption for a given load current will be used as a performance indicator [14] to compare the use of the ES control-based MEPT algorithm to other control techniques mentioned below.

It is worth mentioning that the energy efficiency of the whole FCHPS (including the power interfaces [15]) depends on HPS architecture and battery charging ratios [16]. So, the series HPS architecture is used here to exploit direct connection of the battery to the DC bus and other advantages shown in Refs. [11,17–19] based on the minimization of the equivalent fuel consumption [11], hysteresis band [17], state machine [18], or fuzzy logic control [19].

The main EMU objective is to efficiently sustain the load demand by controlling the FC power flow. Consequently, the maximum FC power must be higher than the maximum load demand. On the other hand, the control inputs for the LF and MEPT controllers from the fueling rates must be determined: the air flow rate (AirFr) and the fuel flow rate (FuelFr). The LF control based on the average (AV) power flows balance and MEPT control based on the ES control scheme are proposed here to reduce the battery stack at minimum and operate the FC stack efficiently. It will be shown that the hydrogen consumption under an unknown load cycle is reduced with 12% compared to the static feed-forward (sFF) control scheme proposed in Ref. [20].

To conclude, using two controllers and two FC input rates means that four topological combinations must be tested here. The references for both controllers will be generated by a Single-Input Double-Output (SIDO) ES control scheme. To compare the results obtained, one of the reference will be generated by the Single-Input Single-Output (SISO) ES control scheme and the other will be generated by the sFF control scheme. All four configurations to fuel the FC stack are compared based on the fuel consumption efficiency, which is the fuel consumption per one kW of the FC net power delivered to the load.

This paper is organized as follows. Section 2 presents the FCHPS system and briefly explains the control loops of the EMU. The experimental work performed in this study is shown in Section 3, as follows: the four possible EMU configurations are detailed in Section 3.1 based on the power flow balance; all the models used in

simulation are briefly shown in Section 3.2; the implementation of the EMU control loops is detailed in Section 3.3. The results obtained are discussed and compared to other EMU strategies in Section 4. Section 5 concludes the paper.

2. FCHPS system

In this paper, a new FC fueling control strategy based on LF and MEPT control loops is presented for the FCHPS system. It is clearly that PEMFC, due to their advantages compared to other FC technologies (such as reduced size and weight, ease of implementation and so on [1,21]), is the best candidate to be used in electric vehicles as a range extender [22]. Also, it is known that the use of the FC stack under dynamic loads, as in the case of FC backup source for a smart home, can destroy the FC stack. Consequently, the FCHPS system must include at least one energy storage device [21,23], which will improve the FCHPS system performance under sharp power profile obtained when high levels are requested on the DC bus [24].

Usually, the hybrid batteries/ultracapacitors ESS topology is used [25]. The batteries used in FCHPS have a higher specific energy than the ultracapacitors, and can sustain an extra power for a period [24,25]. Thus, the semi-active hybrid ESS topology based on bidirectional power convertor to the ultracapacitors stack is usually used due to the compromise of high performance obtained (the ultracapacitors stack SOC can have the maximum available range to dynamically compensate the power flow balance) at reduced cost (only a power converter is used) [15]. So, this semi-active hybrid ESS topology is chosen in this paper, too.

Fig. 1 shows the architecture of the FCHPS system which is composed of: (1) FC stack; (2) ESS (only the battery stack is shown in this Figure); (3) equivalent load; (4) boost converter; (5) ES controllers which form the SIDO ES control scheme; (6) LF control block; and (7) auxiliary services and control modules. For example, in mobile FC application (Fig. 1), the traction motor drives and the braking system are modeled by the equivalent load. If the FCHPS is used as a backup source for a smart home (grid connected), then the equivalent load will also have an unknown power profile. A sharp power profile will be set to test the FCHPS under all EMU strategies proposed.

The EMU is partially shown in Fig. 1 through the LF and MEPT control loops. If the switch is on the sFF position, then the FuelFr input is classically controlled based on the sFF control scheme [20].

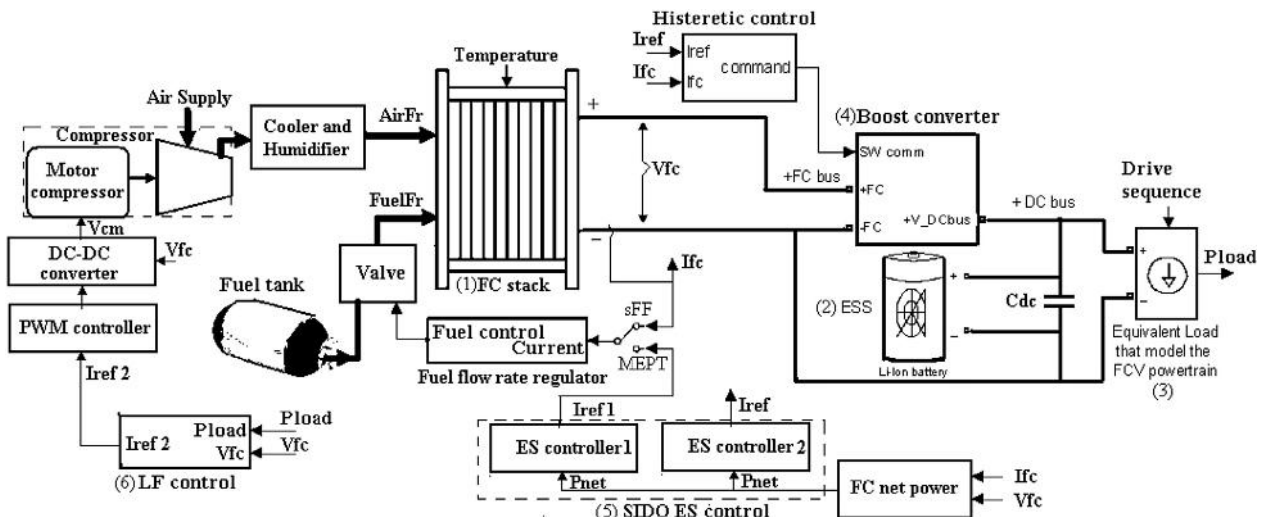


Fig. 1. The FCHPS system.

If the switch is on the MEPT position, then the FuelFr input is efficiently controlled based on the ES controller 1, having as input the FC net power (P_{net}) and as output the reference current 1 (I_{ref1}). The second ES controller has as input the same signal, the FC net power (P_{net}), and as output the reference current (I_{ref}) that controls the FC power flow delivered to the load via boost power converter. The SIDO ES control scheme generates both references for the LF and MEPT control loops, ensuring the efficient operation of the FCHPS.

In fact, the conceptual scheme presented in Fig. 1 integrates both simulation diagrams shown in Fig. 2(a and b), which are developed in detail using MATLAB – Simulink® simulation environment (see Section 3). The mathematical and electrical models of the FCHPS system are presented in Section 4.

The FC stack is the primary energy source of the FCHPS in all four possible configurations proposed to fuel the FC stack. The FC stack will deliver power on the DC bus (to load and ESS), except the stages of the regenerative load profile (for example the braking and deceleration phases or grid connection phases for the mobile and smart home applications, when the load power flow is negative). The FC stack will operate in standby-mode during these stages to avoid the complex start-up procedure. The load power during these stages will charge the batteries stack and, if the electrolyzer is available, this must be started when the battery SOC attains the higher limit set by the EMU strategy [11].

The FC stack uses the fuel (hydrogen) and air (oxygen) rates to optimally supply the load demand based on the LF and MEPT control loops. The hydrogen valve is controlled via the FuelFr regulator. The air is supplied by the air compressor controlled via the DC–DC converter which is PWM controlled in the LF control loop (see Fig. 2).

The FC ancillaries (auxiliary services and control modules) has an important role in avoiding the oxygen starvation phenomenon [10,26], which destroys in time the FC stack [1,2]. Moreover, if they are appropriately controlled, then the hydrogen consumption may be reduced even under unknown load cycles that can produce uncertainties in FC operating parameters [8,27]. One of the ancillaries that needs to be powered is the air compressor system. This is powered by a fraction of the FC power, reducing the net power delivered by the FC stack [10]. It can be noted that the power consumption of the ancillaries is not linear with the FC stack power [13], so that an optimal approach of the EMU design must be used [28,29]. Cheap FC energy may be produced at low FuelFr and high AirFr, but the last value needs higher speed for the compressor, which means an increase in the power fraction delivered to the compressor. Thus, the FC net power decreases. The maximum of the FC net power will be found and tracked by the MEPT algorithm based on the ES control scheme [13], Perturb and Observe (P&O) method [2] or other type of searching algorithm [29].

The FC voltage is boosted via unidirectional boost converter to the standard DC bus. Bidirectional Z-Source Inverter (ZSI) can produce any desired AC output voltage [30], being competitive for the FC vehicle [31,32].

The voltage on the DC bus, u_{dc} , was set to 200 V in this study, which is also the nominal voltage of the Li-ion batteries stack. The DC bus can be modeled as a capacitor, C_{DC} , and the equivalent load as controlled current sources [33]. The voltages range for the ultracapacitors stack must be lower than the voltage on the DC bus. The ultracapacitors stack ensures the dynamic power compensation on the DC bus by using linear and nonlinear control techniques via the bidirectional buck-boost converter [23].

The reference current 2, I_{ref2} , is computed based on the AV value of load power, P_{Load} . The fueling rate must be limited to avoid the fuel and oxidant starvation [4,34]. Gas starvation may also appear during the high slopes of the load profile [26]. So, understanding of

the FCHPS dynamic behavior is a key factor in designing the EMU strategies [23,35,36].

3. Experimental work

3.1. The EMU strategies to control the fueling rates

The dynamic behavior of the DC bus is given by the power flow balance:

$$C_{dc}u_{dc}du_{dc}/dt = p_{ESS} + \eta_{boost}p_{netFC} - p_{Load} \quad (1)$$

where p_{ESS} , p_{netFC} , and p_{Load} are the power of the ESS, FC system, and equivalent load, and η_{boost} is the energy efficiency of the boost converter. The AV value of (1) is:

$$0 = P_{ESS} + \eta_{boost}P_{netFC} - P_{Load} \quad (2)$$

The charge-sustaining mode for the ESS is obtained if the LF control ensures $P_{ESS} = 0$. So, and the AV value of the FC current is given by (3):

$$0 = \eta_{boost}P_{netFC} - P_{Load} \Rightarrow I_{FC(AV)} = P_{Load}/(V_{FC}\eta_{boost}) \quad (3)$$

The EMU strategies proposed in this paper (see Fig. 2) are based on MEPT and LF controllers, which generate the reference currents (I_{ref} , I_{ref1} and I_{ref2}) to optimally supply the FC stack via the FuelFr and AirFr regulators.

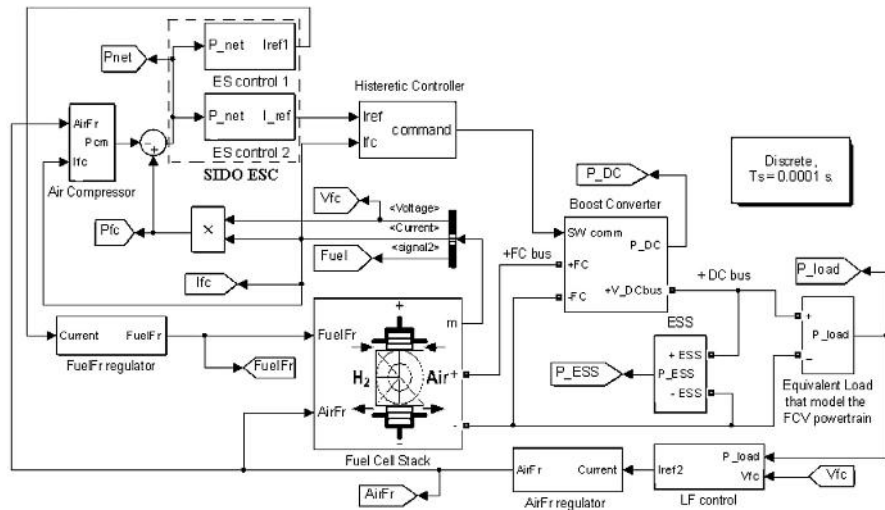
If the value given by (3) is set for the reference current 2, I_{ref2} , then the first two fueling configurations will be obtained by using the reference current 1, I_{ref1} , for the FuelFr regulator (Fig. 2a) or AirFr regulator (Fig. 2b). These configurations will be compared based on the following performance indicators: (1) the fuel consumption efficiency, and (2) increase in the FC net power. The advantage of the MEPT control against the sFF control is shown maintaining the LF control for the same fueling regulator. Thus, other two fueling configurations will be obtained by using the FC current, I_{FC} , for the FuelFr regulator (Fig. 2c) or AirFr regulator (this topology is not shown being excluded from comparison after the first tests).

The reference current (I_{ref}) is the input of the hysteretic control for boost converter used in all fueling configurations.

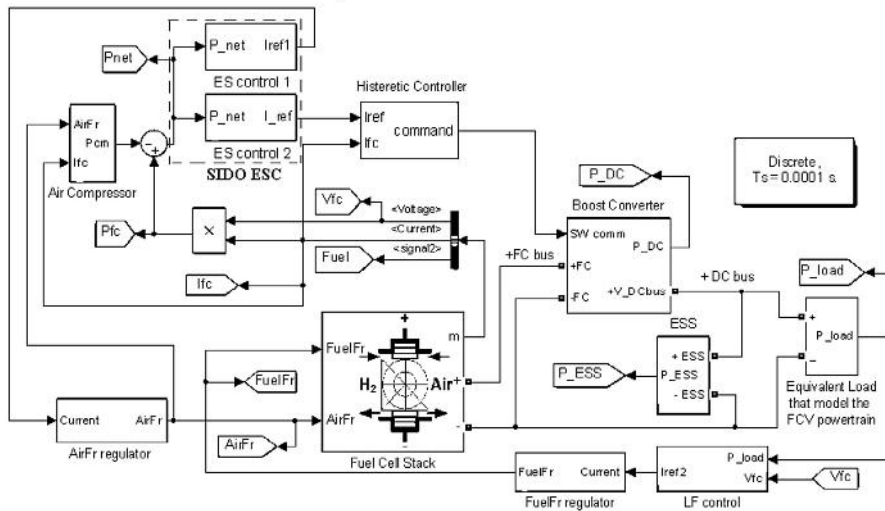
For example, the EMU strategy based on LF and MEPT control loops for the AirFr and FuelFr regulators (shown in Fig. 2a) works as follows. After the start-up procedure, the FC stack is fueled based on present level of the load power and generates power. The SIDO ES controller generates the reference currents (I_{ref} and I_{ref1}) based on the present level of the FC net power using the ES control algorithm which is briefly presented in Section 4.5 and detailed in Refs. [37,38]. The LF control block generates the reference current 2 (I_{ref2}) based on the next level of the load power using (3). The fueling rates are updated based on the reference currents (I_{ref1} and I_{ref2}) via FuelFr and AirFr regulator.

The above operation will run in real time based on the short response (high search speed) of the ES control scheme [38]. For example, if the load power is constant, then the stationary values of the fueling rates will be found in a short time (few milliseconds; depending on the step level of load demand) with about 99.9% stationary accuracy [38]. If the load power is not constant, then the new values of the fueling rates will be computed based on the real time optimization algorithm explained above.

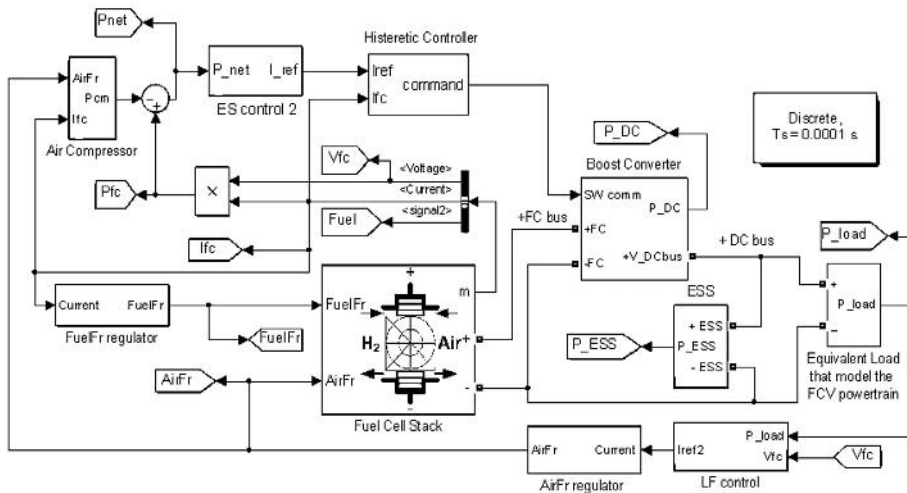
The search speed of the proposed ES control scheme is higher, being limited to safe slopes recommended for the FC power profile [26] via a slope limiter. The DC bus voltage is maintained at 200 V



a. LF and MEPT control loops for the AirFr and FuelFr are based on SIDO ES controller



b. LF and MEPT control loops for the FuelFr and AirFr are based on SIDO ES controller



c. LF and MEPT control loops for the AirFr and FuelFr are based on SISO ES and sFF controllers, respectively

Fig. 2. The simulation diagrams for proposed EMU strategies to control the fueling rates.

by controlling the bidirectional power flow exchanged by the ultracapacitors stack with the DC bus.

So, the contributions at the level of the FCHPS topologies are the following: (1) two advanced fueling configurations are proposed and analyzed in comparison with the sFF control, which is usually used in practice [23,26]; (2) the LF control is proposed to operate the ESS in charge-sustaining mode, being simpler to be implemented compared to wavelet techniques shown in Ref. [8]; (3) the fueling configurations without MEPT control are easy to be adapted on commercially solution based on sFF control [20] due to the simple signal processing operations made by the LF control block; (4) the MEPT – based fueling configuration has the same performance as the EMU strategy based on efficiency map shown in Ref. [35]. Further contributions will be highlighted in Conclusion section based on the results obtained here.

3.2. Used models

3.2.1. Fuel cell system

The FC stack produces electrical energy by a chemical reaction without emitting any gas. In comparison with other FC types, PEMFC is the best option for FCHPS because of its high-energy density of the hydrogen which is the ideal gas to store renewable energy overcapacity on plug-in fueling station. Thus, the FCHPS can be operated indefinitely only by refueling it with hydrogen, like as the diesel generator with gasoline, but only emitting water vapor. The PEMFC has significant advantages, including no emissions, low operating temperature, high efficiency, and capacity to rapidly adjust its power to the power demand [26], but the main problem of the gas starvation phenomenon remains and further research must be made [34]. Furthermore, the cost of the PEMFC stack and auxiliary components has decreased in the last decade to competitive prices [39,40]. The auxiliary components such as compressor, hydrogen tank, humidifier, air cooler, and so on are energy consuming devices from the power delivered by the FC stack, p_{FC} . So, the FC net power is given by (4):

$$P_{netFC} = P_{FC} - P_{aux} \quad (4)$$

where p_{aux} is the power requested by the auxiliary components.

The FC system includes the PEMFC stack, auxiliary components, EMU, protection and safe circuits, so it is obvious that it is a complex system. A lot of research has been carried out in this direction [34,41]. In this paper, the model of the dynamic FC system included in the SimPowerSystems library of the Matlab – Simulink® will be considered [42]. A 6 kW/45 V PEMFC system was chosen. The FC net power characteristic for the FuelFr and AirFr values of 50 lpm and 300 lpm is shown in Fig. 3. The main FC parameters are also shown in Fig. 3. The MEP is about 5400 W, but it is obvious that MEP is difficult to be tracked under unknown dynamic load. Besides the complex behavior of the PEMFC stack, which includes modeling of mass transport processes, the different dynamics of the auxiliary components have effect to the p_{aux} power, affecting the behavior of the overall system. So, the P_{netFC} is difficult to be predicted and could be tracked based on the MEPT control loop [13].

The main power consumer among the auxiliary components is the air compressor (up to 80% power required by all auxiliary components [43]). Furthermore, in comparison with the time constants of the PEMFC stack and air compressor, the thermal management loop is with at least two order of magnitude slower and it can be neglected in the FC system time scale [41]. Consequently, besides the PEMFC stack model mentioned above, the compressor model showed in Fig. 4 will be used in simulation.

The power of the air compressor, P_{cm} , is computed based on (5) [27].

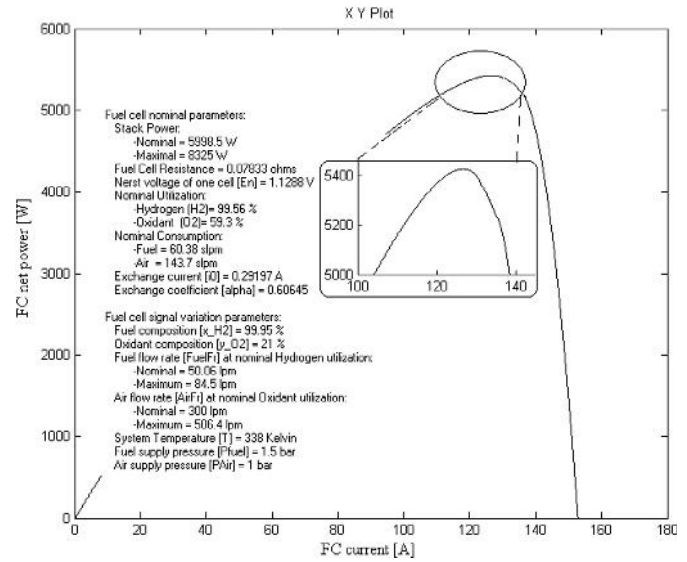


Fig. 3. The FC net power characteristic for the nominal FuelFr and AirFr values and the FC parameters used in simulation.

$$P_{cm} = I_{cm} \cdot V_{cm} = (a_2 \cdot AirFr^2 + a_1 \cdot AirFr + a_0) \cdot (a_1 \cdot I_{FC} + a_0) \quad (5)$$

where $a_0 = 0.6$, $a_1 = 0.04$, $a_2 = -0.00003231$, $b_0 = 0.9987$, and $b_1 = 46.02$.

The compressor dynamics is modeled through a 2nd order system [27] or a dynamic system of higher order [2]. The static gain easily adjusts the power of the air compressor to the different levels of power of all auxiliary components in order to check if the MEPT and LF control schemes proposed are dependent on this power level. For example, if the static gain is set to 0.45, then the P_{cm} power is about 1 kW for nominal FC operating conditions, and this represents a power level in the usual power range that is up to 20% of the FC power available [44]. The FC net power surface is shown in Fig. 5 for different FC operating conditions. The FC net power characteristics via AirFr variable are shown in Fig. 6 to mark the MEPs values.

3.2.2. Energy storage system

FCHPS must use an ESS in order to satisfy the power flows balance (1) under dynamic load [23]. The safe FC power profile means limited slopes, values up to recommended maximum [26,27]. The ESS is better to include batteries and ultracapacitors in a hybrid active or semi-active topology [21,25]. The batteries stack

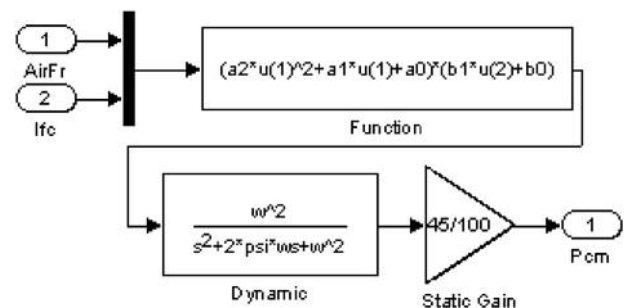


Fig. 4. The diagram of compressor model.

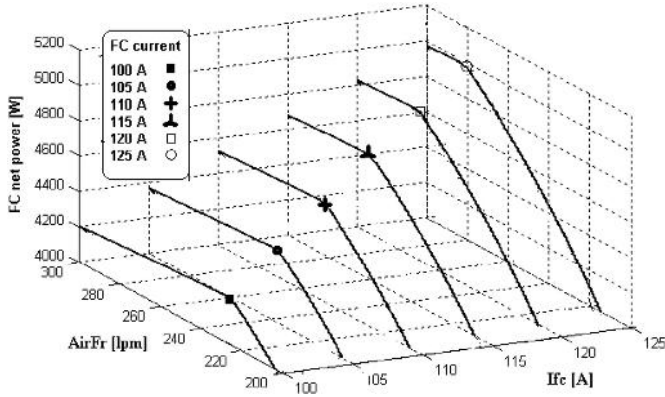


Fig. 5. The FC net power surface.

is connected directly to the DC bus in this study based on hybrid semi-active ESS topology (see Fig. 7).

The ESS recovers energy during the stages of regenerative load power flow due to its reversible capacity to be charged and discharged during charge & discharge cycles. This number of cycles is limited for all types of batteries and practically unlimited for the ultracapacitors.

The ultracapacitors stack is connected to the DC bus via a bidirectional DC–DC converter in order to decrease the number of ultracapacitor cells in series. Thus, the FC system and ultracapacitor stack operate as active controlled power sources. The batteries stack operates as passive controlled energy sources ensuring the power flow balance (1).

3.2.2.1. Battery. The ESS must include a batteries stack due to its high energy density in comparison with the ultracapacitors stack. Different battery types are used in HPS applications [45]. The lithium-ion batteries are a good option for transportation applications (including hybrid, electric and FC vehicles) due to their performances. In this paper, the generic model of the dynamic batteries stack included in the SimPowerSystems library of the Matlab-Simulink® will be considered [42]. Note that an initial SOC of 80% has been considered for the lithium-ion battery with the nominal voltage of 200 V and rated capacity of 100 Ah. Of course, this low capacity of the lithium-ion battery can be set because it is operated in charge-sustaining mode. The battery's parameters

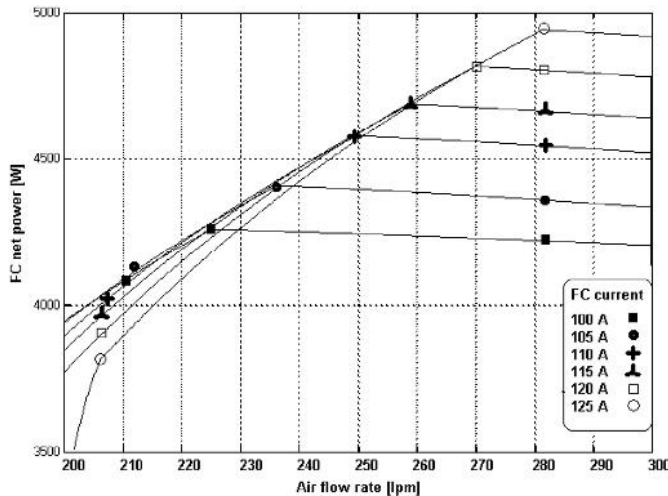


Fig. 6. The FC net power characteristics.

were preset to the value computed based on the battery type and nominal values.

3.2.2.2. Ultracapacitor. The power load profile (used here to cover both mobile and stationary FCHPS applications) includes sharp pulses, which are dynamically compensated by the ultracapacitor stack. The ultracapacitor can be modeled based on electric circuits [46] and non-electric models [47]. Non-electric models are based on computational algorithms [48] and neuronal networks, having the disadvantage of being connected to the electrical circuit via a controlled current source. Thus, the classical electric circuit model was used in the simulation performed in this paper, which includes the equivalent series and parallel resistors (ESR and EPR), and a capacitor (C) that can be identified from the product datasheets. The initial voltage of 100 V has been considered for the 100 F ultracapacitors stack with the ESR of 0.1 Ω and EPR of 10 k Ω .

3.2.3. DC–DC converters

As mentioned in the previous section, two DC–DC power converters are used to interface the FC and ultracapacitors stacks. The FC unidirectional power flow is mainly controlled in the LF control loop and adjusted in the MEPT control loop. The unidirectional DC–DC power converter is of boost type because the FC voltage is lower than 200 V, being in range 40–65 V for a load variation from full load to light load. The AV value on DC bus of the FC power flow is:

$$P_{DC(AV)} = \eta_{boost} P_{netFC} \Rightarrow \eta_{boost} = P_{DC(AV)} / P_{netFC} \quad (6)$$

The bidirectional power flow from the ultracapacitors stack is controlled by the buck-boost converter to stabilize the DC voltage at $V_{DCref} = 200$ V.

The converters are modeled using power devices included in SimPowerSystems® [42].

3.2.4. The equivalent load

The objective of this research work is to evaluate the EMU control strategies proposed for the FCHPS under an unknown load cycle. The power load profile used here tries to cover both mobile and stationary FCHPS applications. So, the equivalent load on the DC bus is modeled as a controlled DC current source connected to the DC bus. Two operating regimes can be set: the constant and the dynamic load.

3.3. Implementation of the EMU control loops

The EMU strategies proposed are mainly based on two controllers for the fueling rates, which include the SIDO ES control scheme (Fig. 8) and the LF controller (Fig. 9). The SIDO ES control scheme is based on the advanced ES control scheme proposed in Ref. [13], where the first tests to find the MEP by direct SIDO ES – based control of both fueling rates were performed without LF control implemented.

In this paper, only one fueling rate is directly controlled by the SIDO ES control scheme to find and track the MEP. The other fueling rate is indirectly controlled by the SIDO ES control scheme based on the LF control loop that sets the FC net power required by the dynamic load.

The FuelFr control could be necessary for some FC applications because the hydrogen tank is limited and it is impractical to recycle the unreacted hydrogen [49]. The air control is usually used to improve the energy efficiency of the FC system [50,51].

Both fueling flow rates are stoichiometrically regulated via the FuelFr and AirFr regulators:

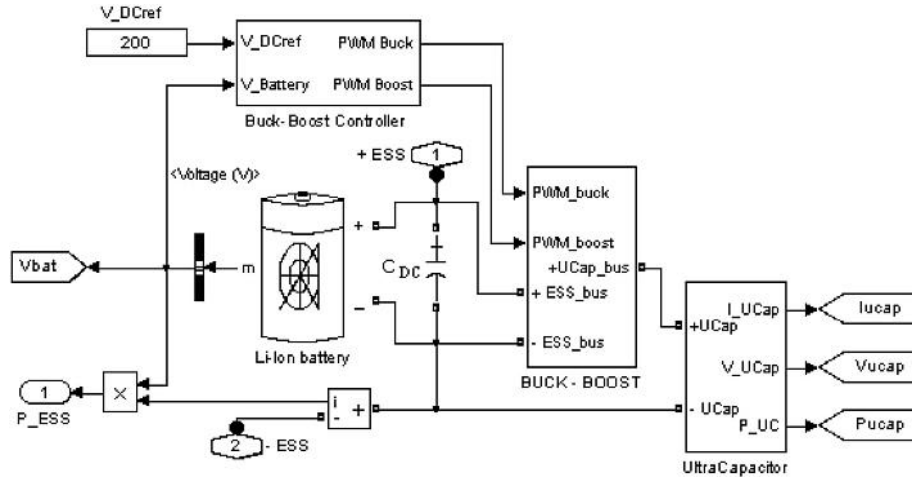


Fig. 7. The diagram of the ESS model.

$$FuelFr = \frac{60000 \cdot R \cdot (273 + \theta) \cdot N_C \cdot I_{ref}(H_2)}{2F \cdot (101325 \cdot P_{f(H_2)}) \cdot (U_{f(H_2)} / 100) \cdot (x_{H_2} / 100)} \quad (7)$$

$$AirFr = \frac{60000 \cdot R \cdot (273 + \theta) \cdot N_C \cdot I_{ref}(O_2)}{4F \cdot (101325 \cdot P_{f(O_2)}) \cdot (U_{f(O_2)} / 100) \cdot (y_{O_2} / 100)} \quad (8)$$

where:

$R = 8.3145 \text{ J/(mol K)}$;

$F = 96,485 \text{ As/mol}$;

N_C represents the number of cells in the series (65);

θ – operating temperature (65° Celsius)

$U_{f(H_2)}$, $U_{f(O_2)}$ – nominal utilization of hydrogen (99.56%) and oxygen (59.3%);

$P_{f(H_2)}$, $P_{f(O_2)}$ – pressure of the fuel (1.5 bar) and air (1 bar);

x_{H_2} , y_{O_2} – composition of fuel (99.95%) and oxidant (21%);

$I_{ref}(H_2)$, $I_{ref}(O_2)$ – reference currents.

The reference currents (I_{ref1} and I_{ref2}) are generated by the SIDO ES control scheme (I_{ref1}) and LF control scheme (I_{ref2}). The reference currents can be associated with Fig. 2 as following: $I_{ref}(H_2) = I_{ref1}$ and $I_{ref}(O_2) = I_{ref2}$ in Fig. 2a, and vice versa in Fig. 2b, where $I_{ref}(H_2) = I_{ref2}$

and $I_{ref}(O_2) = I_{ref1}$. In Fig. 2c, the sFF control is applied to the FuelFr input, which means $I_{ref}(H_2) = I_{FC}$ (because the FC current is a manageable variable). The AirFr value is regulated based on the LF controller ($I_{ref}(O_2) = I_{ref2}$) to evaluate the advantage of the MEPT control used in Fig. 2a, in comparison with the sFF control used in Fig. 2c. In sFF control method [20] it can be noted that both FuelFr and AirFr inputs are regulated through the FC current based on (7) and (8).

The second reference current generated by the SIDO ES (I_{ref}) is used by the hysteretic controller of the boost converter to harvest all the FC power available for the fueling rates set. The FC current tracks the I_{ref} reference current within a hysteresis band of the hysteretic controller. The hysteretic control is also used to regulate the voltage on the DC bus at 200 V. The nonlinear hysteretic control was chosen because it is easy to be implemented. Furthermore, the stabilization of the voltage on the DC is not the main goal of the present paper. Note that the SIDO ES control scheme has as input the FC net power in order to track the MEP in all operating conditions.

3.3.1. The SISO ES control scheme

The diagram of the Single-Input Single-Output (SISO) ES control scheme is shown in Fig. 8. The equations of the SISO ES control scheme are the following [52]:

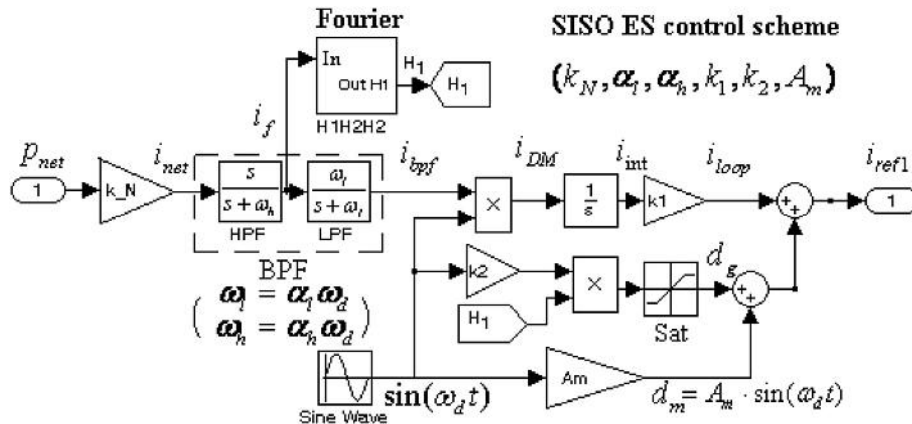


Fig. 8. The diagram of the SISO ES control scheme.

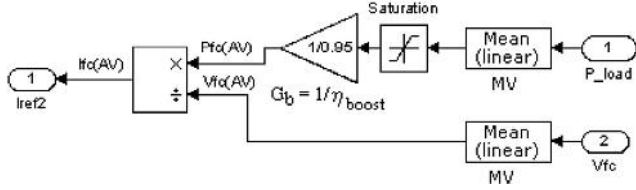


Fig. 9. The diagram of the LF controller.

$$i_{netFC} = k_N \cdot p_{netFC} \quad (9)$$

$$\begin{aligned} \dot{i}_{hpf} &= -\omega_h i_{hpf} + \omega_h i_{netFC}, \quad i_f = i_{netFC} - i_{hpf}, \\ \dot{i}_{BPF} &= -\omega_l i_{BPF} + \omega_l i_f, \end{aligned} \quad (10)$$

$$i_{DM} = i_{BPF} \cdot \sin(\omega_d t) \quad (11)$$

$$\dot{i}_{int} = i_{DM} \quad (12)$$

$$i_{loop} = k_1 i_{int} \quad (13)$$

$$d_g = k_2 H_1 \sin(\omega_d t), \quad d_m = A_m \sin(\omega_d t) \quad (14)$$

$$i_{ref1} = i_{loop} + d_g + d_m \quad (15)$$

where Equations (9)–(15) represent the FC net current, the band pass filter (including the i_{hpf} variable of the high-pass filter (HPF)), the modulator, the integrator, the gained variable in the ES loop, the H_1 – gained and the minimum dithers, and the current reference.

Besides the signals, which are highlighted on Fig. 8, the following notations have been used (including the value used in simulation):

- $f_d = \omega_d/2\pi$ is the dither frequency (100 Hz)
- k_1 – the ES loop gain ($k_1 = 4f_d = 400$);
- k_2 – the dither gain (2);
- k_N – the normalization gain ($k_N = 1/V_{FC} = 1/45$);
- ω_l and ω_h – the cut-off frequencies of the band pass filter (BPF), where $\omega_l = \alpha_l \omega_d$, $\alpha_l = 5.5$, and $\omega_h = \alpha_h \omega_d$, $\alpha_h = 0.1$;
- H_1 – the magnitude of fundamental harmonic of the FC net current;
- A_m – the minimum amplitude of the dither (0.001);
- $*$ – the convolution operator.

The optimization problem based on the ES control can be defined as:

Maximize:

$$P_{net} = J(x, I_{ref(H2)}, I_{ref(O2)}, I_{Load}) \quad (16)$$

Subject to:

$$\dot{x} = f(x, I_{ref(H2)}, I_{ref(O2)}, I_{Load}), \quad x \in X \quad (17)$$

where $I_{ref(H2)}$ and $I_{ref(O2)}$ are the control inputs, I_{Load} is the disturbance input, and f is a smooth function that represents the dynamics of the FC stack based on states model. Note that the state vector, x , can be of a 9th [20] or 6th [53] order.

The orthogonal signals $s_{d2} = \cos(\omega_d t)$ will be used for the second scheme of ES control in order to generate the I_{ref} reference current

Table 1

The results for the simulation diagrams shown in Fig. 2.

I_{load} [A]	15	30	15	30	15	30
	FC net power [W]		Fuel consumption [lpm]		Fuel consumption efficiency [lpm/kW]	
Simulation diagram	P_{net1}	P_{net2}	F_1	F_2	R_1	R_2
Fig. 2a	3800	6200	38	66.5	10	10.7
Fig. 2b	2750	5170	25	58.5	9	11.3
Fig. 2c	3400	5500	38	66.5	11.17	12.09

Table 2

The performance indicators: I_{ab} and I_{ac} .

I_{load} [A]	15	20	25	30
I_{ab} [%]	38.2	33.1	25	19.9
I_{ac} [%]	11.7	12	12.3	12.7

based on the same simulation parameters: $\omega_d = 2\pi \cdot 100$, $k_N = 1/45$, $\omega_h = 0.1\omega_d$, $\omega_l = 5.5\omega_d$, $k_1 = 4f_d$, $k_2 = 2$, $A_m = 0.001$.

3.3.2. The LF controller

The diagram of the LF controller is shown in Fig. 9. The AV block computes the mean value over a running window of one dither period. The saturation block is used to set the lower limit at the standby power value, P_{FCmin} , during the phases of the regenerative load power flow, light load or without load. The upper limit set the maximum FC power, P_{FCmax} . The energy efficiency of the boost converter can be set to be constant (for example, 0.95) or estimated based on (6). Thus, considering (3), the I_{ref2} reference current is estimated based on (18):

$$I_{ref2} = I_{FC(AV)} = P_{Load(AV)} / (V_{FC(AV)} \cdot \eta_{boost(AV)}) \quad (18)$$

The proposed EMU strategies were tested using the MATLAB-Simulink®.

4. Results and discussion

4.1. Constant load

The voltage on the DC bus is stabilized to $V_{DCref} = 200$ V. Thus, the load power profile is set by the load current profile.

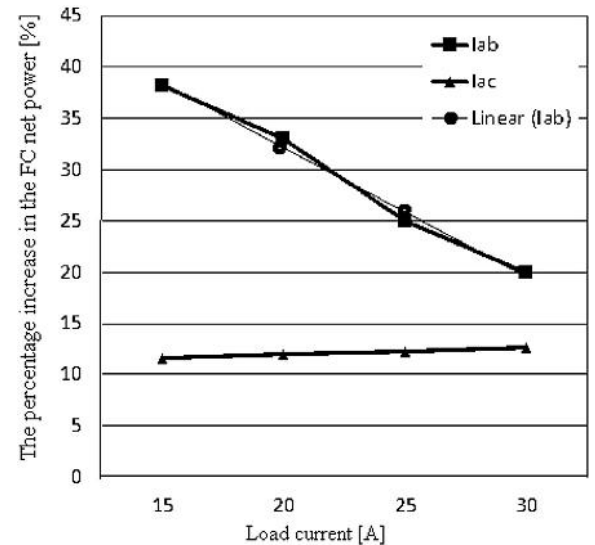


Fig. 10. The percentage increase in the FC net power.

First, the load power is set as constant in all diagrams from Fig. 2. The values of the FC net power (P_{net}) and fuel consumption (F) are given in Table 1 for load current of 15 A and 30 A. The fuel consumption efficiency ($R = F/P_{\text{net}}$) is computed in the last two columns of Table 1.

The percentage increase in the FC net power, $I_{ab} = 100 \cdot (P_{\text{net}(a)} - P_{\text{net}(b)})/P_{\text{net}(b)}$, is computed in Table 2 for the EMU strategy based on load following via the FuelFr (Fig. 2a) and AirFr (Fig. 2b). The percentage increase in the FC net power, $I_{ac} = 100 \cdot (P_{\text{net}(a)} - P_{\text{net}(c)})/P_{\text{net}(c)}$, is also computed in Table 2 for the EMU strategies that are both based on load following via the AirFr input (Fig. 2a and c).

The following remarks can be pointed out from the results shown in Tables 1 and 2:

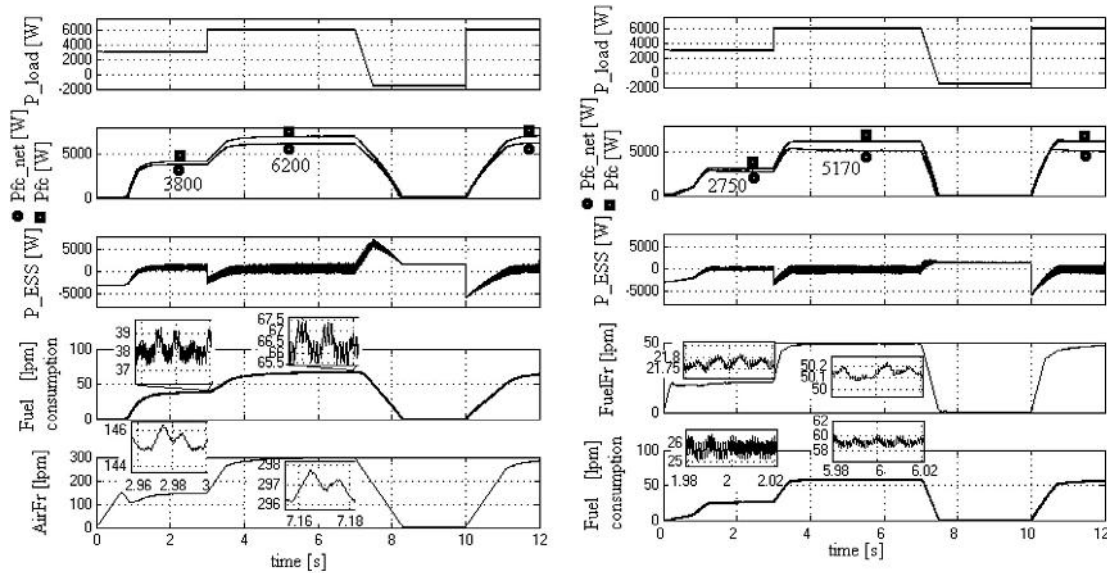
- The fuel consumption efficiency for the EMU strategy based on LF control of the AirFr input is less dependent on the load level (see

first row of Table 1) because this changes directly the level of the AirFr input in the load following loop (not that of the FuelFr input, which is only adjusted by the ES control in order to track the MEP).

- The fuel consumption efficiency for the EMU strategy based on the LF control of the FuelFr input is more dependent on the load level (see second row of Table 1) because this changes directly the level of the FuelFr input in the load following loop.

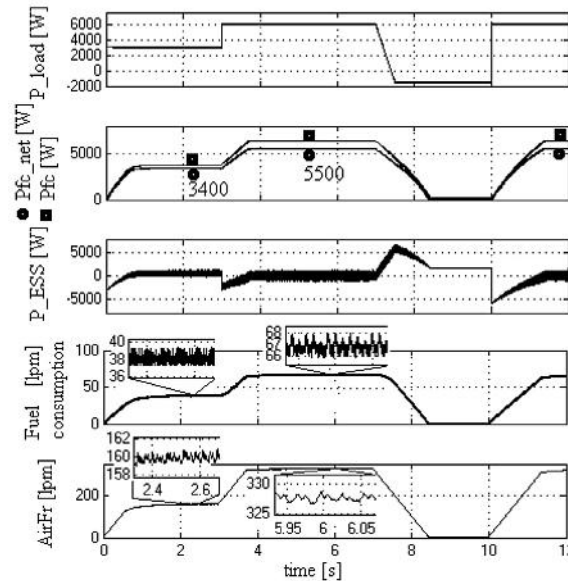
It is obvious that it is difficult to compare these EMU strategies based on the fuel consumption efficiency. The average value of the results shown in Table 1 is about 10.3 and 10.7 for the EMU strategy based on the FuelFr and AirFr load following control, respectively. Thus, the increase in the FC net power will be used to compare these two EMU strategies.

- The percentage increase in the FC net power, $I_{k(ab)} = 100 \cdot (P_{\text{net}(a)} - P_{\text{net}(b)})/P_{\text{net}(b)}$, $k = 1, 2$, is of 38.2% ($I_{1(ab)} =$



a. The results for the simulation diagram shown in Figure 2a

b. The results for the simulation diagram shown in Figure 2b



c. The results for the simulation diagram shown in Figure 2c

Fig. 11. The results for the simulation diagrams shown in Fig. 2.

$100 \cdot (3800 - 2750) / 2750$) and 19.9% ($I_{2(ab)} = 100 \cdot (6200 - 5170) / 5170$) for the EMU strategy based on load following via AirFr input in comparison with the one based on load following via the FuelFr input (see Table 1, first and second row that are related to the results from the simulation diagrams shown in Fig. 2a and b). Thus, the EMU strategy based on the load following control via the AirFr input is more efficient than the one based on the load following control via the FuelFr input. Moreover, it can be seen that the ratio of the percentage increases is about $I_{1(ab)} / I_{2(ab)} \cong 1.91$ for a ratio of the load currents of $15/30 = 1/2$. The percentage is dependent on the load level, having values in range 38%–20% for the load current in range 15 A–30 A. The I_{ab} performance indicator decreases approximately linearly with the increase of the load current, but only in this range can be made this approximation (see Table 2 and the trend line on Fig. 10).

So, the EMU strategies that are both based on load following via the AirFr input (see Table 1, first and third row) must be further compared.

- The opportunity to use the ES control instead of the sFF control should be based on an evaluation of both performance indicators because the cost of implementation of the ES controller (or other MEPT controller) is low in the entire cost of the EMU and the advantages are obvious. First, the fuel consumption efficiency for the ES control is better than that for the sFF control under different load levels (see Table 1, first and third row). Secondly, the percentage increase in the FC net power, $I_{k(ac)} = 100 \cdot (P_{netk(a)} - P_{netk(c)}) / P_{netk(c)}$, $k = 1, 2$, for the ES and sFF control is of 11.7% ($I_{1(ac)} = 100 \cdot (3800 - 3400) / 3400$) and 12.7% ($I_{2(ac)} = 100 \cdot (6200 - 5500) / 5500$), respectively. Thus, the EMU strategy based on a MEPT control is more efficient than that based on the sFF control. Besides, it can be seen that the ratio of the percentage increase is about $I_{1(ac)} / I_{2(ac)} \cong 0.92$. The I_{ac} performance indicator is less dependent on the load level, having values in range 11.7%–12.7% for the load current in range 15 A–30 A (see Fig. 10).

4.2. Dynamic load

The power profile of the dynamic load is set using the following sequence of the load currents:

Time sequence [s]: [0 2.99 3 7 7.5 10 10.01 12]

Load currents sequence [A]: [15 15 30 30 –7.5 –7.5 30 30].

This load power profile is considered for all diagrams shown in Fig. 2 (see first plot on Fig. 11). Note that the FC system operates in standby power regime during the phases of the regenerative load power flow (from about 8.2 to 10 s) to avoid the complex procedure of starting (see second plot on Fig. 11). The batteries stack of the ESS is charged during this phase because the electrolyzer start-up procedure is not implemented here, but the batteries stack operates in charge-sustaining mode the rest of the time (see third plot on Fig. 11).

The fueling rates are limited through the rate limiters included in both FuelFr and AirFr regulators (see last two plots on Fig. 11) in order to avoid the oxygen starvation phenomena. Consequently, the power flow balance (1) written in instantaneous values is mainly sustained by the ultracapacitors stack.

The values of the FC net power and fuel consumption (F), which are given in Table 1 for a load current of 15 A and 30 A (which means a load power of 3000 W and 6000 W), are shown in the plots of Fig. 11 during the stationary regimes. The output of the LF controller controls are the AirFr (Fig. 2a and c) and FuelFr (Fig. 2b)

values obtained based on the AV FC power. Finally, it can be noted that the main advantages of the EMU strategies based on the LF and MEPT control loops are the following: (1) the ESS operates in charge-sustaining mode and (2) FC stack operates efficiently close to the MEP. Thus, the FC and batteries stacks size can be reduced at minimum, with direct implications in the size and cost of the FCHPS.

5. Conclusion

The load following control of the FCHPS via one of the fueling rates is analyzed in this paper in order to decide which option can be efficiently implemented. To further increase the energy efficiency of the FCHPS, the other fueling rate was controlled based on a MEPT control scheme. Consequently, this study was conducted to identify the optimal control configuration for the AirFr and FuelFr inputs based on the LF and MEPT controllers. The first conclusion based on the tests performed here for all possible configurations is with respect to AirFr – based LF control: this reduces the dependence of the FCHPS efficiency by the load profile. The second conclusion regarding the LF control is the following: the ESS will operate in charge-sustaining mode and the size of the batteries stack can be reduced at minimum, with direct implications in the size and cost of the FCHPS. The third conclusion is related to the opportunity to implement a MEPT control instead of the sFF control: the FC net power increases with more than 12% based on the results obtained, if the MEPT control was implemented. These conclusions clarify the advantages of the AirFr/FuelFr – based LF/MEPT control scheme in comparison with the other control topologies analyzed here. The next work will be focused on implementing this EMU strategy based on two FC stacks to further reduce the size of the FCHPS: the FC stacks will sustain (1) the nominal load and (2) difference to the maximal load.

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